

## Nickel(II)–Cyclam: an Extremely Selective Electrocatalyst for Reduction of CO<sub>2</sub> in Water

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CO<sub>2</sub> is electroreduced efficiently to CO on a mercury cathode, in the presence of [Ni<sup>II</sup>(cyclam)]<sup>2+</sup>; even in pure water, the selectivity for reduction of CO<sub>2</sub> vs. that of H<sub>2</sub>O is huge.

The reduction of CO<sub>2</sub> is important in converting this abundant carbon source into organic products. On metal cathodes, the direct electrochemical reduction of CO<sub>2</sub> generally occurs at highly negative potentials.<sup>1</sup> Recently, several molecular electrocatalysts have been proposed that diminish the overvoltage; they are mainly based on nitrogen-containing macrocyclic complexes of cobalt or nickel.<sup>2–5</sup> A difficulty arises in the selectivity of reduction in that the presence of H<sub>2</sub>O is necessary<sup>4</sup> and H<sub>2</sub> is generally one of the major products. Until now, one of the only selective electrocatalysts reported seems to be a rhenium(I) complex, operating in a mixed solvent.<sup>6</sup> We report here that (1,4,8,11-tetra-azacyclotetradecane)nickel(II) {[Ni<sup>II</sup>(cyclam)]<sup>2+</sup>} is a selective electrocatalyst for the reduction of CO<sub>2</sub> to CO, even in pure water; in addition, the reaction is effective at potentials *ca.* 0.5 V below the thermodynamic value [CO<sub>2</sub>/CO: *E*° = -0.41 V vs.

normal hydrogen electrode (N.H.E.) at pH = 5]. Some results are listed in Table 1.

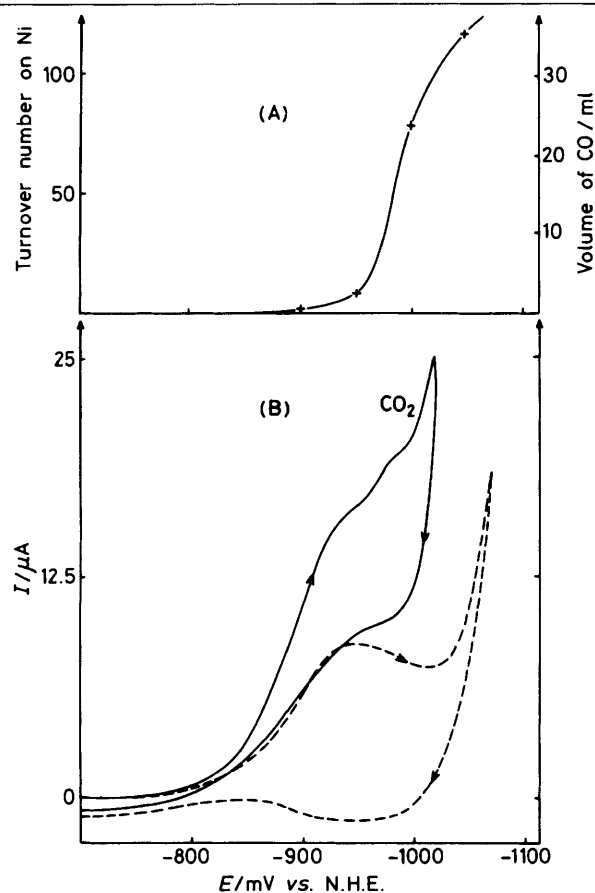
The experimental data clearly show that (i) without electrocatalyst or with NiCl<sub>2</sub>, only H<sub>2</sub> can be detected (runs 1 and 2), (ii) in the presence of [Ni<sup>II</sup>(cyclam)]<sup>2+</sup>, the electroreductive process is effective at -0.9 V, the velocity of the reaction being remarkable (turnover frequency *ca.* 32 h<sup>-1</sup>) at -1.05 V (run 6), (iii) [Ni<sup>II</sup>(cyclam)]<sup>2+</sup> is quantitatively recycled (overall turnover numbers *ca.* 10<sup>2</sup> in runs 5 and 6), and (iv) the Faradaic yields are almost quantitative for runs 5 and 6, confirming the high selectivity of the process. Taking into account the respective concentrations of CO<sub>2</sub> (< 0.1 M) and H<sub>2</sub>O (*ca.* 55 M) in the medium, the actual selectivity for reduction of CO<sub>2</sub> vs. that of H<sub>2</sub>O is higher than 10<sup>6</sup>.

The catalytic effect of [Ni<sup>II</sup>(cyclam)]<sup>2+</sup> was demonstrated by cyclic voltammetry, as shown in Figure 1. Clearly, an

**Table 1.** Electrocatalytic reduction of CO<sub>2</sub> by [Ni<sup>II</sup>(cyclam)]<sup>2+</sup> in water.<sup>a</sup>

| Run | Electrocatalyst                      | <i>E</i> (V vs. N.H.E.) | Total volume <sup>b</sup> of CO produced (ml) | Turnover frequency (h <sup>-1</sup> ); <sup>c</sup> overall turnover of Ni | Average current efficiency <sup>d</sup> /% | Volume of H <sub>2</sub> produced/ml; H <sub>2</sub> : CO in gas produced |
|-----|--------------------------------------|-------------------------|-----------------------------------------------|----------------------------------------------------------------------------|--------------------------------------------|---------------------------------------------------------------------------|
| 1   | —                                    | -1.05                   | < 0.05                                        | —                                                                          | —                                          | 0.36; > 10                                                                |
| 2   | NiCl <sub>2</sub> ·6H <sub>2</sub> O | -1.05                   | < 0.05                                        | —                                                                          | —                                          | 1.6; > 30                                                                 |
| 3   | Ni(cyclam)Cl <sub>2</sub>            | -0.90                   | 0.4                                           | 0.3; 1.2                                                                   | 36                                         | < 0.01; < 2 × 10 <sup>-2</sup>                                            |
| 4   | Ni(cyclam)Cl <sub>2</sub>            | -0.95                   | 3.6                                           | 2.9; 10.8                                                                  | 82                                         | < 0.01; < 3 × 10 <sup>-3</sup>                                            |
| 5   | Ni(cyclam)Cl <sub>2</sub>            | -1.00                   | 23.7                                          | 18; 77.5                                                                   | 99                                         | < 0.01; < 5 × 10 <sup>-4</sup>                                            |
| 6   | Ni(cyclam)Cl <sub>2</sub>            | -1.05                   | 35.6                                          | 32; 116                                                                    | 96                                         | < 0.01; < 3 × 10 <sup>-4</sup>                                            |

<sup>a</sup> CO<sub>2</sub> (99.995% purity) saturated solutions (75 ml H<sub>2</sub>O at 25 °C; pH ca. 4.1) containing the electrocatalyst (1.7 × 10<sup>-4</sup> M) and KNO<sub>3</sub> (0.1 M) were placed in a gas-tight electrolysis cell; the working electrode (18 cm<sup>2</sup>) was mercury (99.99999% purity). The total volume occupied by the gases in the electrolysis cell was 86 ml. The gases were analysed by g.c. <sup>b</sup> After 4 h of electrolysis. <sup>c</sup> Turnover numbers are calculated from mol of CO produced per mol of electrocatalyst. <sup>d</sup> Current efficiency  $\rho: \rho = \frac{2n_{CO} \times 96500}{C}$ ,  $n_{CO}$ : mol CO produced,  $C$  = coulombs passed during the run.



**Figure 1.** (A) Amount of CO produced in 4 h of electrolysis as a function of applied potential; experimental conditions: see footnote a, Table 1. (B) Cyclic voltammograms of [Ni<sup>II</sup>(cyclam)]<sup>2+</sup> (2 × 10<sup>-3</sup> M) in H<sub>2</sub>O. Full line: CO<sub>2</sub> saturated solution (measured pH = 4.1); dashed line: argon degassed solution (pH = 4.1, adjusted with dilute HNO<sub>3</sub>). Hanging mercury electrode; support electrolyte: KNO<sub>3</sub> (0.1 M); scan rate = 600 mV/s; room temperature.

important electrocatalytic current is observed when CO<sub>2</sub> is present; in MeCN, the reversibility of the [Ni<sup>II</sup>(cyclam)]<sup>2+</sup>/[Ni<sup>I</sup>(cyclam)]<sup>+</sup> couple<sup>7</sup> was lost by addition of CO<sub>2</sub>. Even at high scan rates (200 V/s), no reoxidation process could be observed after reduction of [Ni<sup>II</sup>(cyclam)]<sup>2+</sup> in water under CO<sub>2</sub>. Without CO<sub>2</sub>, the [Ni<sup>II</sup>(cyclam)]<sup>2+</sup>/[Ni<sup>I</sup>(cyclam)]<sup>+</sup> couple is reversible in aqueous KClO<sub>4</sub> ( $E^\circ = -1.33$  V vs. N.H.E.), whereas reversibility is lost in dilute KNO<sub>3</sub>; indeed [Ni<sup>II</sup>(cyclam)]<sup>2+</sup> is an electrocatalyst for reduction of nitrate to NH<sub>4</sub><sup>+</sup>.

Slight changes in the conditions used or in the nature of the catalyst have a significant influence on the course of the

reaction: (1) the reaction becomes much less efficient when the pH is increased in a KHCO<sub>3</sub>/K<sub>2</sub>CO<sub>3</sub> buffer (pH = 10.6; 0.25 M), only trace amounts of CO and formate are formed after electrolysis at -1.05 V vs. N.H.E. CO<sub>2</sub> is thus the real substrate. (2) Surprisingly, among a large number of tetra-aza complexes of nickel investigated, only [Ni<sup>II</sup>(cyclam)]<sup>2+</sup> displays exceptional electrocatalytic properties; unsaturated macrocyclic compounds or open chain complexes (containing 2,3,2-teten, 3,2,3-teten, or tren)<sup>†</sup> are very poor catalysts. Nickel complexes of saturated substituted tetra-aza 14 membered rings are acceptable electrocatalysts, but they are not selective for reduction of CO<sub>2</sub> vs. that of H<sub>2</sub>O.<sup>5</sup> The particularity of [Ni<sup>II</sup>(cyclam)]<sup>2+</sup> is due to its macrocyclic structure, making the reduced compound resistant to decomplexation;<sup>8</sup> in addition, steric factors are likely to be determinant: the highly accessible metal centre of [Ni<sup>I</sup>(cyclam)]<sup>+</sup> reacts more readily with CO<sub>2</sub> than would that of, for instance, [Ni<sup>I</sup>(L)]<sup>+</sup>, L being 5,5,7,12,12,14-hexamethyl-1,4,8,11-tetra-azacyclotetradecane.<sup>9</sup> On the other hand, if the metal centre is hindered, it might react with a small substrate like a proton, making the process less specific with respect to reduction of CO<sub>2</sub>.

In conclusion, these preliminary results indicate that the unencumbered complex, [Ni<sup>II</sup>(cyclam)]<sup>2+</sup>, is an active and selective electrocatalyst for reduction of CO<sub>2</sub> in aqueous medium, whereas acyclic or substituted compounds have drastically different properties as catalysts.

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<sup>†</sup> 2,3,2-teten = 1,3,7,9-tetra-azanonane; 3,2,3-teten = 1,4,7,10-tetra-azadecane; tren = 1,3,5-triaza-3-(2-aminoethyl)pentane.